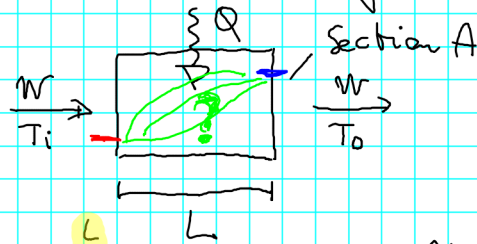


15/05/2019

1
State variable for flowing thermal elements



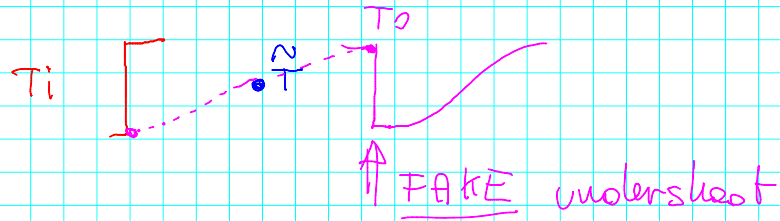
$$E(t) = \int_0^L c_p T(x,t) \rho A dx = \frac{N}{T} \cdot c_p M$$

↑ who is this guy?

2 Suppose

$$\tilde{T} = \frac{T_i + T_o}{2}$$

↑ state variable \Rightarrow NO JUMP!



Hence we take $\tilde{T} = T_o$

But we need to know the sign (direction) of \dot{w}

3

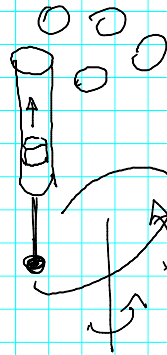


plate
angle \Rightarrow piston stroke \Rightarrow flow rate

Heat exchanger: two streams of fluid, a wall separating them

C → H
C → H
co-current

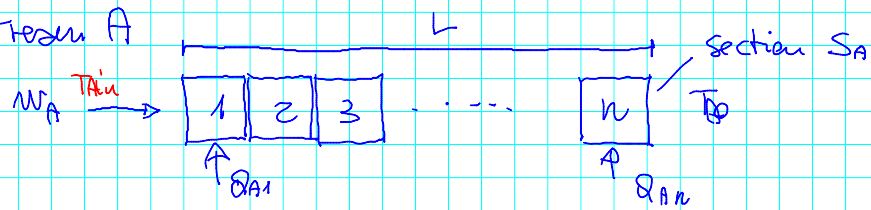
C → H
H ← C
counter-current

Fluid → air
counter-cross

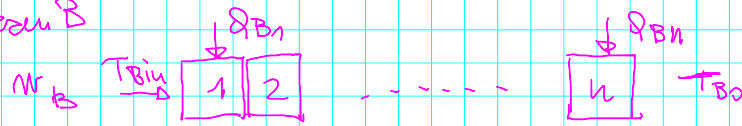
shell-tube
Shell
tubes

FINITE-VOLUME APPROACH (known Flow direction)

5 Stream A



Stream B

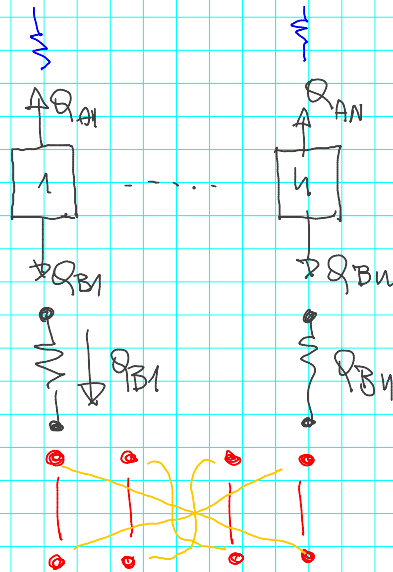


$$\rho_A c_A S_A \frac{L}{n} \frac{dT_{Ai}}{dt} = \dot{m}_A c_A T_{Ai-1} - \dot{m}_A c_A T_{Ai} + Q_{Ai}, \quad T_{Ao} = T_n$$

$\uparrow T_{Ai} \text{ if } i=1$

Analogous

Overall:



$$C_w \rho_w V_w \frac{dT_{wi}}{dt} = -Q_{Ai} - Q_{Bi}$$

U-M-Fluid
exchange

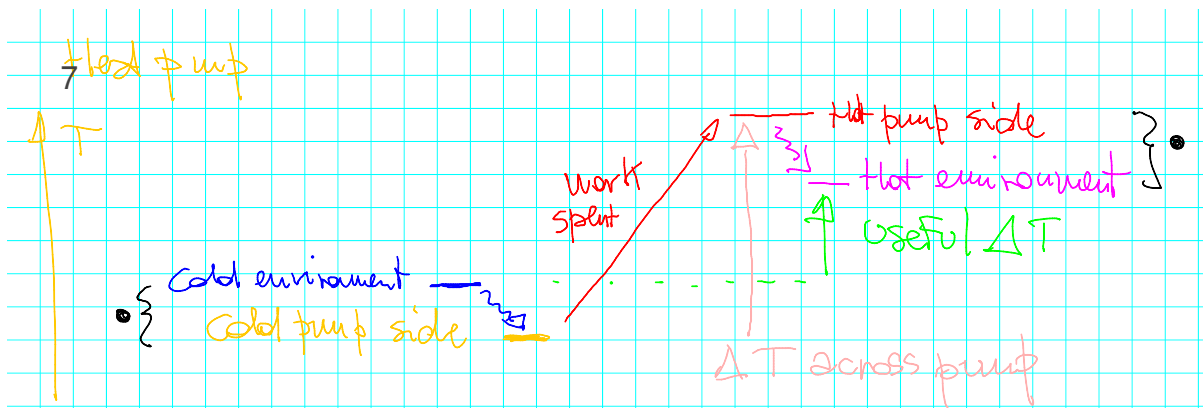
$$Q_{Bi} = G_{Bi} (T_{wi} - T_{Bi})$$

connection
element

A side analysis

Co-current

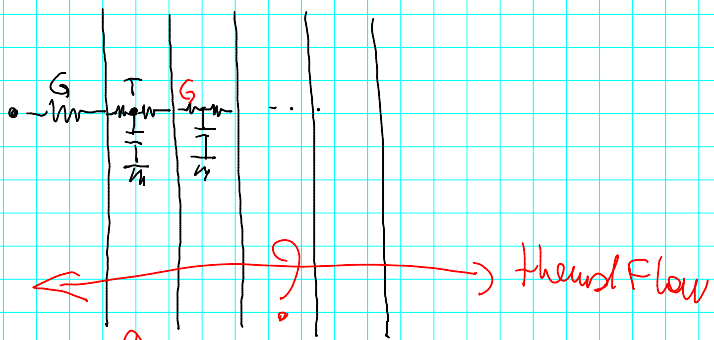
Counter-current



- these ΔT can be reduced by more efficient exchangers \Rightarrow space, money

containing elements

8



↑ each layer

$\rho, c, V \Rightarrow$ CAPACITY

λ conductivity $\Rightarrow G = \frac{\lambda \cdot \text{Area}}{\text{Thickness}}$